

REMARKS

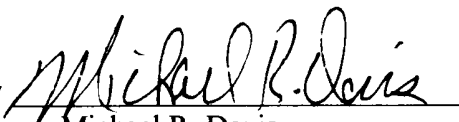
The specification has been amended to insert a cross-reference to the international application on which the present U.S. application is based.

The claims have been amended to avoid their improper multiple dependency.

Attached hereto is a marked-up version of the changes made to the claims by the current Preliminary Amendment. The attached page is captioned "Version with markings to show changes made."

Respectfully submitted,

Ola OLSVIK et al.

By 

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VERSION WITH MARKINGS TO SHOW CHANGES MADE

IN THE CLAIMS:

3(amended). Method according to [claims 1-2] claim 1,
c h a r a c t e r i z e d i n that the ratio $H_2O:CO$ in the shift process is from 1 to 9.

4(amended). Method according to [claims 1-3] claim 1,
c h a r a c t e r i z e d i n that the ratio $H_2O:CO$ in the shift process preferably is from 1.5 to 4.

5(amended). Method according to [claims 1-4] claim 1,
c h a r a c t e r i z e d i n that the pressure in the CO_2 -rich gas stream after the separation unit is
from 1 to 100 bar.

6(amended). Method according to [claims 1-5] claim 1,
c h a r a c t e r i z e d i n that the pressure in the CO_2 -rich gas stream after the separation unit is
from 5 to 50 bar.

7(amended). Method according to [claims 1-6] claim 1,
c h a r a c t e r i z e d i n that the carbon part in the H_2 -rich gas stream is from 1 to 20 % by
volume.

8(amended). Method according to [claims 1-7] claim 1,
c h a r a c t e r i z e d i n that the carbon part in the H_2 -rich gas stream is from 5 to 15 % by
volume.

9(amended). Method according to [claims 1-8] claim 1,
c h a r a c t e r i z e d i n that the natural gas in step a) is supplied with an oxygen rich gas.

10(amended). Method according to [claims 1-8] claim 1,
c h a r a c t e r i z e d i n that the natural gas in step a) is supplied with air/oxygen enriched air.

11(amended). Method according to [claims 1-8] claim 1,
c h a r a c t e r i z e d i n that the reformer reactor preferably is a partial oxidation reactor.

12(amended). Method according to [claims 1-11] claim 1,

characterized in that the reformer reactor particularly is an autothermal reformer.

15(amended). Method according to [claims 1-14] claim 1,
characterized in that the gas stream out of the reformer has a temperature within the
interval from 800 to 1200°C.